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Zirconia-Based Compositions for Use in Passive NO_x Adsorber Devices

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(54) **ZIRCONIA-BASED COMPOSITIONS FOR USE IN PASSIVE NOX ADSORBER DEVICES**

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See application file for complete search history.

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(57) **ABSTRACT**

A passive NO_x adsorbent includes: palladium, platinum or a mixture thereof and a mixed or composite oxide including the following elements in percentage by weight, expressed in terms of oxide: 10-90% by weight zirconium and 0.1-50% by weight of least one of the following: a transition metal or a lanthanide series element other than Ce. Although the passive NO_x adsorbent can include Ce in an amount ranging from 0.1 to 20% by weight expressed in terms of oxide, advantages are obtained particularly in the case of low-Ce or a substantially Ce-free passive NO_x adsorbent.

19 Claims, No Drawings

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ZIRCONIA-BASED COMPOSITIONS FOR USE IN PASSIVE NOX ADSORBER DEVICES

TECHNICAL FIELD

This disclosure relates to treating gas streams so as to remove nitrogen oxides (NOx) therefrom and in particular, to passive NOx adsorbents (PNA) that store NOx at lower temperatures and then release the NOx at higher temperatures.

TECHNICAL BACKGROUND

Urea-SCR (Selective Catalytic Reduction) is a well-known solution for treating the NOx emissions from diesel engines, but requires the exhaust temperatures to be above 200° C. [1]. The heating rate on diesel engines/exhaust can be relatively slow, and this results in a delay between switching the engine on and being able to dose urea and effectively remove NOx by SCR (“cold-start” period). The NOx emissions during this cold start period comprise a large portion of the total emissions during the FTP-75 and NEDC test protocols for example, and this has significant implications for real world driving.

In Europe, the legislated NOx limits for diesel vehicles have been constantly falling since the introduction of the Euro standard, and the current Euro VI limit is 0.080 g/km (September 2014).

One solution is to utilize a “passive NOx adsorbent” (PNA) material upstream of the SCR catalyst, which is capable of storing NOx below 200° C. (i.e., during the cold start period) and then releasing it above this temperature (i.e., once the SCR catalyst is active).

Standard lean NOx trap materials (e.g., Pt/Ba/Al₂O₃) which require the oxidation of NO to NO₂ are useful at higher temperatures but do not tend to store NOx efficiently below 150° C. In this regard, an alternative class of materials are necessary that are more active at lower temperatures (from ambient up to 200° C.).

In addition to the low temperature NOx storage capability, PNA materials must also have suitable thermal stability. Depending on the location (e.g., on DOC), it may experience temperatures up to 800-850° C. (hydrothermal) under high engine load conditions. The PNA will always be upstream of the SCR catalyst but may be downstream of a filter, which could be regenerated actively or passively. Hence the PNA must maintain its low temperature activity after such thermal excursions.

Further to these thermal stability demands, candidate PNA materials should also be robust to the presence of sulfur-containing species in the exhaust gas. This implies that the materials have a relatively low propensity for adsorbing sulfur species, but also tend to de-sulfate under suitable conditions (e.g. preferably below 700° C. in lean conditions).

U.S. Pat. No. 8,105,559 refers to the use of palladium on ceria (Pd—CeO₂) as an effective PNA candidate. NOx is allegedly stored effectively at 120° C., 160° C. or 200° C., and is allegedly desorbed almost immediately upon ramping the temperature. However, no data is provided on the effect of sulfur in the feed gas.

U.S. Pat. No. 8,920,756 refers to the use of an Ag/Al₂O₃ component in combination with another material to create a passive NOx adsorber system. The second material may contain manganese, but only in combination with ceria, and this is likely to be inherently sulfur-intolerant. In addition to this, the function of the second component is to store NOx

once the temperature is above 190° C. (NOx during the initial cold start period being stored on the Ag/Al₂O₃ component).

U.S. Pat. No. 9,687,811 discusses the use of various materials/combinations for use in the PNA application. Specific mention is made of manganese, but this is used/added as a bulk Mn₃O₄ component (i.e., not part of a solid solution) which is expected to lead to poor thermal stability and low sulfur-tolerance. Further to this, the Mn₃O₄ component is always added in combination with a ceria component.

Zhao-shun Zhang and co-workers (*Appl. Cat. B: Environmental*, 165 (2015) 232-244) investigated the addition of manganese into a model lean NOx trap (Pd/Ba/Al₂O₃). They demonstrated enhanced NO oxidation activity but required temperatures above 300° C. for efficient NOx storage.

Li-Hong Guo and co-workers (*Catal. Today*, June 2017) also investigated model manganese oxide systems under more relevant NOx storage conditions (i.e., <200° C.) and found that NOx could be stored effectively. However, although MnO₂ had the greatest NOx storage capacity, the strong adsorption of NOx meant that desorption was more difficult, and Mn₂O₃ showed more facile NOx release. So, when designing manganese-containing PNA materials, one should consider the state of the Mn species and the impact of other components of the mixed or composite oxide on this. Oxidation of NO to NO₂ is not always beneficial, with surface nitrites being generally less stable than nitrates, and thus more easily desorbed.

U.S. Patent application publication No. 2009/0191108 refers to the use of praseodymia-zirconia mixed oxides (optionally containing ceria) in NOx trapping applications for lean burning internal combustion engines. Although the materials showed improved sulfur-tolerance compared to Ba/Al₂O₃ reference (after rich regeneration at 550° C.), there is no low temperature activity promoting element (such as a transition metal) and these materials require temperatures of 200-300° C. for suitable NOx storage.

And finally, the palladium-on-zeolite system has received a lot of attention for the PNA application, such as U.S. published patent application No. 2012/0308439. Although efficient low temperature NOx storage is observed, the palladium usage can be quite high (>50 g/ft³) which has cost implications, and these materials also tend to adsorb hydrocarbons which may or may not be advantageous.

SUMMARY OF THE DISCLOSURE

This disclosure features a composition for a passive NOx adsorbent comprising Zr-based mixed or composite-oxides. The passive NOx adsorbent includes at least one of the following: a transition metal (e.g., Mn, W, Fe) and a lanthanide series element (e.g., Pr). In some instances structural promoters, for example, an oxide of Y, La or Nd, may be used to improve the thermal durability of Zr-based mixed or composite-oxides [*Applied Catalysis*, 1991; *Topics in Catalysis*, July 2004].

The passive NOx adsorbents of this disclosure compensate for a deficiency in performance of conventional catalysts in removing NOx in gasoline and diesel engine exhaust from motor vehicles. The passive NOx adsorbents herein are able to store or adsorb NOx from the lean exhaust gas stream at lower temperatures (e.g., below 200° C.) at a point when conventional catalysts do not perform well. Then, above 200° C. the passive NOx adsorbents herein release or desorb the NOx at a point when the conventional catalysts can perform well. For example, the passive NOx adsorbent of

the disclosure releases the NO_x at temperatures above 200° C. to a downstream and different SCR catalyst device which reduces the NO_x to nitrogen gas so as to satisfy stringent NO_x emission regulations for motor vehicles.

A first aspect of this disclosure features a passive NO_x adsorbent including: palladium, platinum or a mixture thereof and a mixed or composite oxide. The mixed or composite oxide includes the following composition: 10-90% by weight zirconium and 0.1-50% by weight of at least one of the following: a transition metal or a lanthanide series element other than Ce.

It should be appreciated that in the mixed or composite oxides of this disclosure, for example, the recited weight percentages of elements on an oxide basis are based on a total weight of the mixed or composite oxide and when combined equal 100%. Further, use of “comprising” transitional claim language does not exclude additional, unrecited elements or method steps. Moreover, the disclosure also contemplates use of “consisting essentially of” transitional claim language, which limits the scope of the claim to the specified materials or steps and those that do not materially affect the basic and novel characteristic(s) of the claimed invention which include the function of the mixed or composite oxide as a passive NO_x adsorbent. When numerical ranges are used, the range includes the endpoints unless otherwise indicated.

Specific features of the first aspect of the disclosure will now be described. The mixed or composite oxide can include at least one of W, Mn and Fe as the transition metal. The transition metal(s) can be present in an amount ranging from 0.1% to 20% by weight of the mixed or composite oxide, on an oxide basis.

Particular mixed or composite oxides include the following: Pr—Zr; Mn—Zr; W—Zr; and Mn—Pr—Zr; any of the foregoing including Fe; and any of the foregoing including optional amounts of Ce or being substantially free of Ce as discussed further in the Summary of the Disclosure below.

In another feature, the mixed or composite oxide can include at least one of Pr, Tb, or a mixture of Pr and Tb, as the lanthanide series element other than Ce.

Yet another feature is that the mixed or composite oxide can include Pr as the lanthanide series element other than Ce, and at least one of the following metals selected from W, Mn, and Fe as the transition metal.

A further feature is that the mixed or composite oxide can include at least one of Y, La and Nd as the lanthanide series element other than Ce, present in an amount of up to 20% by weight, in particular, in an amount ranging from 0.5 to 20% by weight. In the case of rare earth elements including at least one of Y, La, Nd, when an amount greater than or equal to 0.5 wt % is recited, this indicates that the element(s) are intentionally added.

Another feature is that the mixed or composite oxide can include Pr and at least one of Y, La and Nd as the lanthanide series element other than Ce in an amount ranging from 0.5% to 20% by weight, and at least one of the following metals selected from W, Mn, and Fe as the transition metal in an amount ranging from 0.1% to 20% by weight.

A further feature is that the mixed or composite oxide can include an element from Group 14 of the Periodic Table (e.g., Si or Sn) in an amount ranging from 0.1 to 20% by weight expressed in terms of oxide.

Other features are that the mixed or composite oxide can include Mn as the transition metal in an amount of 0.1 to 20% by weight and Pr as the lanthanide series element other than Ce, in an amount of 0.5 to 30% by weight, the total amount of Mn and Pr being not more than 50% by weight.

The following specific features may apply to the above feature. In one feature, the mixed or composite oxide can further include at least one of W and Fe as the transition metal. In addition, the mixed or composite oxide can further include at least one of Y, La and Nd as the lanthanide series element other than Ce. Moreover, the mixed or composite oxide can include an element from Group 14 of the Periodic Table (e.g., Si or Sn) in an amount ranging from 0.1 to 20% by weight expressed in terms of oxide.

The mixed or composite oxide of the passive NO_x adsorbent can include Ce in the following amounts: not more than 20% by weight expressed in terms of oxide; in particular, in an amount ranging from 0.1% to 20%; further ranging from 0.1 to less than 5%; further still ranging from 0.5 to less than 5%; and in particular, the passive NO_x adsorbent can be substantially free of Ce.

The passive NO_x adsorbent as a fresh material can have a minimum NO_x storage capacity of 7.5 μmol/g after 5 minutes at 120° C.

Further, the passive NO_x adsorbent as an aged material can have a minimum NO_x storage capacity of 5 μmol/g after 5 minutes at 120° C.

Another feature is a passive NO_x adsorbent according to the first aspect in which the mixed or composite oxide includes Mn as the at least one transition metal and includes optional element X, wherein when element X is present it is: at least one of Ce; or Pr as the lanthanide series element other than Ce, with a minimum fresh NO_x storage capacity of at least 40 μmol/g after 5 minutes at 120° C.

Yet another feature is a passive NO_x adsorbent according to the first aspect in which the mixed or composite oxide includes Mn as the at least one transition metal and optional element X, wherein when element X is present it is: at least one of Ce; or Pr as the lanthanide series element other than Ce, with a minimum aged NO_x storage capacity of at least 19 μmol/g after 5 minutes at 120° C.

Another feature is a passive NO_x adsorbent according to the first aspect in which the mixed or composite oxide includes Mn as the at least one transition metal and Pr as the lanthanide series element other than Ce, with a minimum fresh NO_x storage capacity of at least 50 μmol/g after 5 minutes at 120° C.

Still further is featured a passive NO_x adsorbent according to the first aspect in which the mixed or composite oxide includes Mn as the at least one transition metal and Pr as the lanthanide series element other than Ce, with a minimum aged NO_x storage capacity of at least 45 μmol/g after 5 minutes at 120° C.

Another feature is a monolithic substrate supporting a washcoat, the washcoat comprising the passive NO_x adsorbent of the first aspect of the disclosure.

Further the passive NO_x adsorbent of the first aspect of the disclosure can be used in combination with a Selective Catalytic Reduction catalyst.

A second aspect of the disclosure features a method for reducing nitrogen oxides (NO_x) present in a lean gas stream including at least one of nitric oxide (NO) and nitrogen dioxide (NO₂), including the following steps. The passive NO_x adsorbent of the first aspect of the disclosure is provided in the lean gas stream. NO_x is adsorbed from the lean gas stream on or in the passive NO_x adsorbent at a temperature below 200° C. NO_x is thermally net desorbed from the passive NO_x adsorbent in the lean gas stream at 200° C. and above. The NO_x is catalytically reduced on a downstream catalyst situated downstream of the passive

NO_x adsorbent, with at least one of the following reductants: a nitrogenous reductant, a hydrocarbon reductant, hydrogen and a mixture thereof.

In one specific feature of the second aspect the lean gas stream emanates from a gasoline fueled or diesel fueled engine.

Many additional features, advantages and a fuller understanding of the disclosure will be had from the Detailed Description that follows. It should be understood that the above Summary of the Disclosure describes the subject matter of the disclosure in broad terms while the following Detailed Description describes the subject matter of the disclosure more narrowly and presents particular embodiments that should not be construed as necessary limitations of the broad subject matter of the disclosure.

DETAILED DESCRIPTION

Fresh Mn-zirconia passive NO_x adsorbents and Mn—Pr-zirconia passive NO_x adsorbents exhibit NO_x storage values after, for example, 5 minutes at 120° C. comparable to those of analogous fresh materials containing Ce but drop off after 15 minutes at 120° C. As known in the art, aging represents expected behavior of a material after being in use for a period of time. Looking at aged PNA materials, the Mn—Pr-zirconia passive NO_x adsorbent compositions of this disclosure exhibit NO_x storage values after all times up to 15 minutes at 120° C. comparable or considerably greater than those of the Ce-containing analogues.

The term “passive NO_x adsorbent (PNA)” as used in this disclosure means an adsorbent disposed in a gas stream, which stores NO_x from the gas stream at temperatures up to 200° C. and releases the stored NO_x into the gas stream at temperatures greater than 200° C. If an SCR catalyst is used, the PNA can be located upstream of the SCR catalyst, for example. When the term “fresh” is used in this disclosure it means an adsorbent material that has only been calcined under such conditions as to decompose any precursor constituents into an “active” form, and hasn’t undergone any accelerated and/or in-use ageing.

Tungstated zirconia (WO₃—ZrO₂) passive NO_x adsorbent material has also been shown to exhibit considerably greater NO_x storage values compared to pure zirconia (in the presence of Pt or Pd, and tested fresh).

Equally important for passive NO_x adsorbents, the stored NO_x can be thermally desorbed from the adsorbent with high efficiency in the working temperature range of 200-350° C. The tungstated zirconia adsorbent discussed above has also been shown to exhibit a greater percentage of the amount of NO_x desorbed to the amount stored compared to other materials presented here. Similarly, the addition of Pr to Mn-zirconia adsorbent has been shown to be beneficial in terms of facilitating thermal NO_x release between 200 and 250° C. compared to non-Pr containing and Ce-containing analogues.

Therefore, comparable properties and even definite advantages are obtained in the passive NO_x adsorbents of this disclosure when avoiding use of Ce, compared to Ce containing compositions. The passive NO_x adsorbents of this disclosure advantageously can limit Ce to the following amounts on an oxide basis: Ce in an amount not more than 20% by weight; Ce in an amount ranging from 0.1 to 20% by weight; Ce in an amount less than 5% by weight; Ce ranging from 0.5% to less than 5% by weight; and in particular, the composition is substantially free of Ce.

While the addition of Fe to Ce-zirconia passive NO_x adsorbent material provides for less overall NO_x storage

compared to a Mn—Ce-zirconia passive NO_x adsorbent material, the Fe-containing adsorbent material exhibits a greater percentage of the amount of NO_x desorbed to the amount stored. By extrapolation, it is believed this desorbing behavior resulting from use of Fe would also be evident in non-ceria containing passive NO_x adsorbent material or low-ceria containing passive NO_x adsorbent material.

The mixed or composite oxide compositions of the passive NO_x adsorbents of this disclosure may include the listed elements as oxides. However, a portion of the elements may be in a form of hydroxides or oxyhydroxides. The passive NO_x adsorbents can be in the form of a powder. Typical characteristics of the PNA powder include: particle size; d₅₀ may range from about 1 μm to about 100 μm, although for washcoated materials the d₅₀ will generally be <10 μm. The surface area of the fresh PNA powder will typically fall in the range 40-250 m²/g. The total pore volume of the fresh PNA powder will typically fall in the range 0.10-1.0 cm³/g. Impurity levels of the fresh PNA powder are <500 ppm of Na or Cl and <0.1% SO₄ typical impurities. Naturally occurring HfO₂ may be present in an amount of 1-2% in the ZrO₂ used in the adsorbents of this disclosure. The PNA powder may be applied as an aqueous washcoat that coats a substrate, for example, onto a monolithic substrate, and in particular, onto a honeycomb shaped monolithic substrate. Examples of monolith coating methods suitable for use in this disclosure can be found in US2011/0268634A1 and WO2017/144493A1, which are incorporated herein by reference in their entireties, although other techniques could be used.

The passive NO_x adsorbents of this disclosure may be used in various gas streams containing NO_x and, in particular, in lean gas streams. An example lean gas stream includes the following components in the indicated percentages by volume: CO₂ about 12%, H₂O about 11%, O₂ about 9%, NO_x 50-1000 ppm, CO 100-500 ppm, PM 1-30 mg/m³, HC 20-300 ppm. One particular application is in an exhaust stream of a gasoline fueled engine of a motor vehicle. Another application is in the exhaust stream of a diesel fueled engine of a motor vehicle. Non-automotive applications such as trains and ships are also relevant with regard to use of the materials of this disclosure, along with stationary emissions sources such as power stations, refineries, and general industrial facilities that generate NO_x.

Given that interest in this type of automotive application is growing (in an effort to decrease cold start emissions from lean-burn engines), the commercial application of these devices can be expected in the near future.

Suitable methods for preparing the passive NO_x adsorbents of this disclosure may include (but are not limited to) the methods described in the following references, all of which are incorporated herein by reference in their entireties:

1. Cauqui, M. A.; Rodriguez-Izquierdo, J. M. *J. Non-Cryst. Solids*, 1992, 147/148, 724. (Sol-gel method);
2. J. A. Navio, et al., *Chem. Mater.* 1997, 9, 1256-1261. (Alkaline precipitation);
3. Kolen'koa Y., et al., *Mater. Sci. Eng. C*, 2003, 23, 1033 (Hydrothermal synthesis);
4. Kasilingam Boobalan, et al., *J. Am. Ceram. Soc.* 2010, 11, 3651-3656 (Combustion method);
5. U.S. Pat. No. 7,431,910;
6. U.S. Pat. No. 7,632,477;
7. U.S. Pat. No. 7,794,687.

The subject matter of the disclosure will now be described by reference to the following examples, which are for

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purposes of illustration and should not necessarily be used to limit the subject matter herein.

Example 1

A portion of tungstated zirconia mixed or composite oxide (15.75% WO_3 /84.25% ZrO_2) (e.g., can be made using the process described in U.S. Pat. No. 7,632,477) was used as a support to make the "Pt—W—Zr" and "Pd—W—Zr" materials. All amounts of compounds in this disclosure are in % by weight that together equal 100% of the composition, unless otherwise indicated. It is assumed the zirconia includes an amount of HfO_2 up to 2% even if this is not indicated.

Pt and Pd were deposited on the support by means of incipient wetness impregnation. The support material was first dried in a vacuum oven at 70° C. overnight then impregnated with an aqueous solution of tetra-amine platinum (II) nitrate (or tetra-amine palladium nitrate). Pt and Pd loadings were kept at 1 wt % for single metal catalysts, the remainder being the mixed or composite oxide. If bimetallic catalysts are used, Pt and Pd can be simultaneously loaded on the support by co-impregnation using a mixture of Pt and Pd tetra-amine nitrate solution. For bimetallic catalysts, Pt and Pd loadings can be 0.5 wt % for each metal, the remainder being the mixed or composite oxide. After drying at 50° C. overnight in a vacuum oven, the impregnated samples were calcined at 500° C. for 3 h.

For some of the Examples and Comparative Example, fresh and aged PNA powders had characteristics recited in Table 3 below.

A microreactor loaded with about 150 mg of PNA powder (free flowing powder, having a particle size of less than 0.2 mm) was employed to study the NO_x adsorption and desorption properties of the adsorbents. In all the cases, a total flow rate of 120 sccm was used, corresponding to a gas hourly space velocity (GHSV) of about 30,000 h^{-1} .

Effluent gases were analyzed using a mass spectrometer (QMS 200). Unless otherwise stated, the adsorbents were first pretreated at the desired NO_x storage temperature under lean gas containing 5% O_2 , 5% CO_2 and 3.5% H_2O until the samples were saturated (based on a comparison of the feed and effluent gas concentrations); typically this required 15 minutes.

NO_x storage was performed at three different temperatures (80, 100 and 120° C.) by adding 300 ppm NO to the lean feed gas. After NO_x storage for a specified period of time, the feed gas was switched to bypass mode and the NO flow was switched off.

When the NO concentration had dropped to zero, the gas was re-directed to the reactor and temperature-programmed desorption was carried out to study NO_x desorption behavior using a ramp rate of 10° C./min from the storage temperature up to 500° C. The results are presented in Table 1.

Comparative Example 1

A portion of undoped zirconia (e.g., can be made using the process described in U.S. Pat. No. 7,794,687) was used as a support to make the "Pt—Zr" and "Pd—Zr" materials and then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

Example 2

A portion of undoped zirconia (same material as used in COMPARATIVE EXAMPLE 1) was first impregnated with

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an aqueous solution of manganese nitrate, then dried and calcined at 500° C. for 3 h. The resulting Mn— ZrO_2 oxide (20.0% MnO_2 /80.0% ZrO_2) was subsequently impregnated with aqueous tetra-amine palladium (II) nitrate and further calcined at 500° C. for 3 h. Pd loading in the catalysts was maintained at 1 wt %.

The material of EXAMPLE 2 was then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

Example 3

A portion of a ceria-zirconia mixed or composite oxide (25.7% CeO_2 /74.3% ZrO_2) (e.g., can be made using the process described in U.S. Pat. No. 7,431,910) was first impregnated with an aqueous solution of manganese nitrate, then dried and calcined at 500° C. for 3 h. The resulting Mn—Ce— ZrO_2 oxide (20.0% MnO_2 /20.6% CeO_2 /59.4% ZrO_2) was subsequently impregnated with aqueous tetra-amine palladium (II) nitrate and further calcined at 500° C. for 3 h. Pd loading in the catalysts was maintained at 1 wt %.

The material of EXAMPLE 3 was then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

Example 4

A portion of manganese-zirconia mixed or composite oxide (13.3% MnO_2 /86.7% ZrO_2) was used as a support for palladium and tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,632,477, which is incorporated herein by reference in its entirety. The results are presented in Table 1.

Example 5

A portion of EXAMPLE 4 (with palladium added) was hydrothermally aged and then tested based on the procedures detailed in EXAMPLE 1. All hydrothermal ageing carried out in this disclosure is under the conditions of 750° C. for 16 hours in 10% O_2 , 5% CO_2 , 5% H_2O , balance N_2 gas. The results are presented in Table 1.

Example 6

A portion of a manganese-praseodymia-zirconia mixed or composite oxide (14.3% MnO_2 /14.0% Pr_6O_{11} /71.7% ZrO_2) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,632,477. The results are presented in Table 1.

Example 7

A portion of a manganese-ceria-zirconia mixed or composite oxide (13.0% MnO_2 /10.0% CeO_2 /77.0% ZrO_2) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910.

Example 8

A portion of a manganese-praseodymia-zirconia mixed or composite oxide (7.0% MnO_2 /13.6% Pr_6O_{11} /79.4% ZrO_2)

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was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,632,477. The results are presented in Table 1.

Example 9

A portion of EXAMPLE 8 (with palladium added) was hydrothermally aged and then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

Example 10

A portion of a manganese-ceria-zirconia mixed or composite oxide (6.3% MnO₂/9.7% CeO₂/84.0% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910. The results are presented in Table 1.

Example 11

A portion of EXAMPLE 10 (with palladium added) was hydrothermally aged and then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

Example 12

A portion of a manganese-ceria-zirconia mixed or composite oxide (20.0% MnO₂/10.0% CeO₂/70.0% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910. The results are presented in Table 1.

Example 13

A portion of EXAMPLE 12 (with palladium added) was hydrothermally aged and then tested based on the procedures detailed in EXAMPLE 1. The results are presented in Table 1.

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Example 14

A portion of an iron-ceria-zirconia mixed or composite oxide (20.0% Fe₂O₃/10.0% CeO₂/70.0% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910. The results are presented in Table 1.

Example 15

A portion of an iron-ceria-zirconia mixed or composite oxide (10.0% Fe₂O₃/10.0% CeO₂/80.0% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910. The results are presented in Table 1.

Example 16

A portion of an iron-ceria-zirconia mixed or composite oxide (5.0% Fe₂O₃/10.0% CeO₂/85.0% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910. The results are presented in Table 1.

Example 17

A manganese-silica-praseodymia-zirconia mixed or composite oxide was prepared (7.0% MnO₂/13.6% Pr₆O₁₁ 5.0% SiO₂/74.4% ZrO₂); analogous to EXAMPLE 8 but with silica present.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,632,477.

Conclusions:

Conclusions drawn from the test results described in the discussed in EXAMPLES 1-16 and COMPARATIVE EXAMPLE 1 are shown in Table 1 and discussed below. In the discussion, amounts of the elements in the mixed or composite oxides are rounded to the nearest whole number.

TABLE 1

Results of testing the Indicated PNA materials for a storage temperature of 120° C. and a desorption time of 15 minutes.							
Material	Amount NO _x Stored at 120° C. (μmol/g)				Amount NO _x Desorbed (μmol/g)		% of Amount Desorbed to Amount Stored
	1 min	2 min	5 min	15 min	15 min <250° C.	15 min <350° C.	15 min <350° C./15 min
Comparative Example 1 (Pt)	4.97	9.71	14.62	29.42	7.56	11.09	38
Comparative Example 1 (Pd)	3.59	5.62	10.73	23.45	8.91	16.81	72
Example 1 (Pt)	3.67	5.01	7.77	12.99	7.26	10.30	79
Example 1 (Pd)	9.42	15.76	24.19	30.65	24.88	29.35	96
Example 2 (Pd)	10.69	21.10	45.73	80.06	32.80	64.61	81
Example 3 (Pd)	10.19	19.19	43.59	92.47	23.23	55.91	60
Example 12 (Pd)	11.10	21.47	53.78	145.78	30.32	102.70	70
Example 13 (Pd)	10.41	18.23	27.30	34.42	15.15	23.71	69
Example 4 (Pd)	10.96	21.65	53.64	126.87	45.73	111.67	88

TABLE 1-continued

Results of testing the Indicated PNA materials for a storage temperature of 120° C. and a desorption time of 15 minutes.							
Material	Amount NO _x Stored at 120° C. (μmol/g)				Amount NO _x Desorbed (μmol/g)		% of Amount Desorbed to Amount Stored
	1 min	2 min	5 min	15 min	15 min <250° C.	15 min <350° C.	15 min <350° C./15 min
Example 5 (Pd)	9.61	13.87	20.10	31.88	14.86	19.96	63
Example 7 (Pd)	10.78	21.24	53.55	136.66	34.44	100.70	74
Example 6 (Pd)	10.70	21.35	53.34	113.94	36.72	75.04	66
Example 8 (Pd)	10.68	21.33	52.88	118.95	36.33	58.74	49
Example 9 (Pd)	10.47	20.62	46.53	69.91	16.26	48.41	69
Example 10 (Pd)	10.76	21.43	53.63	114.76	41.26	75.03	65
Example 11 (Pd)	10.62	20.30	31.95	37.69	22.81	36.23	96
Example 14 (Pd)	2.79	4.87	10.55	25.59	12.86	22.77	89
Example 15 (Pd)	2.99	5.30	11.22	27.75	13.53	24.11	87
Example 16 (Pd)	2.99	5.11	10.79	26.62	16.58	27.83	100

Example 1 (Pd)

The Pd—W—Zr material exhibits greater NO_x storage at 120° C. at all times explored compared to the Pd—Zr material (see COMPARATIVE EXAMPLE 1 (Pd)) and greater percentage of the amount NO_x desorbed to the amount stored. In particular, the Pd—W—Zr material exhibits an amount of NO_x desorbed to the amount stored of 96%.

Example 2 (Pd)

The Pd—Mn(20)-Zr material exhibits NO_x storage values after 5 minutes at 120° C. comparable to those of the Pd—Mn(20)-Ce(21)-Zr material (see EXAMPLE 3 (Pd)) but less storage after 15 minutes at 120° C. However, the Pd—Mn(20)-Zr material exhibits considerably better NO_x desorption at all temperatures explored relative to the amount stored, compared to the Pd—Mn(20)-Ce(21)-Zr material. This illustrates a definite advantage over materials that include Ce, for use as passive NOx adsorbents.

Example 4 (Pd)

The Pd—Mn(13)-Zr material exhibits NO_x storage values after 5 minutes at 120° C. comparable to those of the Pd—Mn(13)-Ce(10)-Zr material (see EXAMPLE 7 (Pd)) but less storage after 15 minutes at 120° C. However, the Pd—Mn(13)-Zr material exhibits a greater percentage of the amount NO_x desorbed to the amount stored. This shows a definite advantage over Ce containing adsorbent material.

Example 6 (Pd)

The Pd—Mn(14)-Pr(14)-Zr material exhibits NO_x storage values after 5 minutes at 120° C. comparable to those of the Pd—Mn(13)-Ce(10)-Zr material (see EXAMPLE 7 (Pd)).

Example 8 (Pd)

The Pd—Mn(7)-Pr(14)-Zr material exhibits NO_x storage values after 5 minutes at 120° C. comparable to that of the Pd—Mn(6)-Ce(10)-Zr material (see EXAMPLE 10 (Pd)).

Example 9 (Pd)

The Pd—Mn(7)-Pr(14)-Zr (HT aged) material exhibits comparable or better NO_x storage values at 120° C. at all times explored with respect to the Pd—Mn(6)-Ce(10)-Zr (HT aged) material (see EXAMPLE 11 (Pd)). In particular, the Pd—Mn(7)-Pr(14)-Zr (HT aged) material of Example 9 (Pd) exhibited the greatest amount of NOx storage of all the aged materials explored in these EXAMPLES and COMPARATIVE EXAMPLES at about 70 μmol/g.

Example 14 (Pd)

While the Pd—Fe(20)-Ce(10)-Zr material exhibits less NO_x storage compared to a Pd—Mn—Ce-zirconia material (e.g. see EXAMPLE 12 (Pd)), the Pd—Fe(20)-Ce(10)-Zr material exhibits a large percentage of the amount of NO_x desorbed to the amount stored. By extrapolation, this behavior resulting from use of Fe would also be evident in non-ceria containing materials.

Example 15 (Pd)

While the Pd—Fe(10)-Ce(10)-Zr material exhibits less NO_x storage compared to a typical Pd—Mn—Ce-zirconia material (e.g. see EXAMPLE 7 (Pd)), the Pd—Fe(10)-Ce(10)-Zr material exhibits a large percentage of the amount NO_x desorbed to the amount stored.

By extrapolation, this behavior resulting from use of Fe would also be evident in non-ceria containing materials.

Example 16 (Pd)

While the Pd—Fe(5)-Ce(10)-Zr material exhibits less NO_x storage compared to a Pd—Mn—Ce-zirconia material (e.g. see EXAMPLE 10 (Pd)), the Pd—Fe(5)-Ce(10)-Zr material exhibits a large percentage of the amount NO_x desorbed to the amount stored. By extrapolation, this behavior resulting from use of Fe would also be evident in non-ceria containing materials.

The disclosure now turns to further examples and a comparative example for illustrating the subject matter of the disclosure, which should not be used to necessarily limit the subject matter herein.

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Example 18

A portion of a praseodymia-zirconia mixed or composite oxide (25.5% Pr₆O₁₁/74.5% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,632,477. The results are presented in Table 2 below.

Example 19

A portion of a ceria-praseodymia-zirconia mixed or composite oxide (20.6% CeO₂/5.1% Pr₆O₁₁/74.3% ZrO₂) was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in U.S. Pat. No. 7,431,910. The results are presented in Table 2 below.

Comparative Example 2

A portion of a high ceria-praseodymia-zirconia mixed or composite oxide (67.9% CeO₂/16.8% Pr₆O₁₁/15.3% ZrO₂) obtained from MEL Chemicals was used as a support for palladium and then tested based on the procedures detailed in EXAMPLE 1.

This mixed or composite oxide can be made using the process described in Applicant's U.S. Pat. No. 7,431,910. The results are presented in Table 2 below.

CONCLUSIONS

Conclusions drawn from the test results described in Examples 18 and 19 and Comparative Example 2 are shown in Table 2 and discussed below.

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TABLE 2

Results of testing the PNA materials for a storage temperature 120° C. and a desorption time of 5 minutes.

Material	Amount NO _x Stored at 120° C. (μmol/g)			Amount NO _x Desorbed (μmol/g)	
	1 min	2 min	5 min	5 min- <250° C.	5 min- <350° C.
Example 18 (Pd)	5.02	8.35	16.78	8.63	13.24
Example 19 (Pd)	4.99	8.03	15.68	5.18	10.15
Comparative Example 2 (Pd)	5.67	10.18	20.65	5.85	7.15

While the praseodymia-zirconia mixed or composite oxide of Example 18 and the ceria-praseodymia-zirconia mixed or composite oxide of Example 19 did not have high storage of NO_x after 5 minutes at 120° C. minutes compared to other materials tested, they exhibited a relatively high amount of NO_x desorbed. Although the high ceria-praseodymia-zirconia mixed or composite oxide of Comparative Example 2 exhibited slightly better storage of NO_x after 5 minutes at 120° C. compared to the adsorbents of Examples 18 and 19, this is for a significant increase in ceria/praseodymia level (and therefore expense) and it exhibited only a comparable or a lesser amount of NO_x desorbed at the temperatures tested (a significant facet of the PNA function).

Table 3 below shows Surface area, total pore volume and crystallite size for fresh and aged PNA material of the indicated EXAMPLES and COMPARATIVE EXAMPLES.

TABLE 3

Characteristics of Fresh and Aged PNA materials of the Indicated EXAMPLES and COMPARATIVE EXAMPLES.

	Fresh			Air Aged (900° C./2 hr)			Hydrothermally aged (750° C./16 hr)	
	SA (m ² /g)	TPV (cm ³ /g)	CS (nm)	SA (m ² /g)	TPV (cm ³ /g)	CS (nm)	SA (m ² /g)	TPV (cm ³ /g)
COMP.	84	0.35						
EXAMPLE 1								
EXAMPLE 3								
EXAMPLE 4	149	0.41	8.2	7	0.03			
EXAMPLE 5	—							
EXAMPLE 6	153	0.40	4.2	25	0.11	16		
EXAMPLE 7	146	0.41	8.3	11	0.05	27		
EXAMPLE 8	95	0.45	11	27	0.12	16		
EXAMPLE 9	—						48	0.24
EXAMPLE 10	98	0.39	9.6	13	0.07	26		
EXAMPLE 11	—							
EXAMPLE 12	103	0.30						
EXAMPLE 13	—						21	0.10
EXAMPLE 14	80							
EXAMPLE 15	67							
EXAMPLE 16	62							
EXAMPLE 17	150	0.63	6.3	46	0.26	11		
EXAMPLE 18	80	0.36	12					
EXAMPLE 19	82	0.34	7.9					
COMPARATIVE EXAMPLE 2	94	0.24	7.1					

SA = Surface Area
 TPV = Total Pore Volume
 CS = Crystallite Size (from XRD)

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Many modifications and variations of the subject matter of the disclosure will be apparent to those of ordinary skill in the art. Therefore, it is to be understood that the subject matter of the disclosure can be practiced otherwise than has been specifically shown and described.

What is claimed is:

1. A passive NO_x adsorbent comprising: palladium, platinum or a mixture thereof and a mixed or composite oxide comprising the following elements in percentage by weight, expressed in terms of oxide: 10-90% by weight zirconium; and 0.1-50% by weight of least one of the following: a lanthanide series element other than Ce, comprising Pr; and a transition metal comprising at least one of the following metals selected from W, Mn, and Fe.

2. A passive NO_x adsorbent according to claim 1 further comprising at least one of Y, La and Nd as said lanthanide series element other than Ce.

3. A passive NO_x adsorbent according to claim 1, comprising Mn as said transition metal in an amount of 0.1 to 20% by weight and Pr as said lanthanide series element other than Ce in an amount of 0.5 to 30% by weight, wherein a total amount of Pr and Mn is not more than 50% by weight.

4. A passive NO_x adsorbent according to claim 3 further comprising at least one of W and Fe as said transition metal.

5. A passive NO_x adsorbent according to claim 3 further including at least one of Y, La and Nd as said lanthanide series element other than Ce.

6. A passive NO_x adsorbent according to claim 3 further comprising an element from Group 14 of the Periodic Table in an amount ranging from 0.1 to 20% by weight expressed in terms of oxide.

7. A passive NO_x adsorbent according to claim 1 comprising Ce in an amount ranging from 0.1% to not more than 20% by weight expressed in terms of oxide.

8. A passive NO_x adsorbent according to claim 1 comprising Ce in an amount ranging from 0.5 to not more than 5% by weight expressed in terms of oxide.

9. A passive NO_x adsorbent according to claim 1 with the proviso that the passive NO_x adsorbent is substantially free of Ce.

10. A passive NO_x adsorbent according to claim 1 with a minimum fresh NO_x storage capacity of 7.5 μmol/g after 5 minutes at 120° C.

11. A passive NO_x adsorbent according to claim 1 with a minimum aged NO_x storage capacity of 5 μmol/g after 5 minutes at 120° C.

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12. A passive NO_x adsorbent according to claim 1 in which the mixed or composite oxide includes Mn as said at least one transition metal and optional Ce, with a minimum fresh NO_x storage capacity of at least 40 μmol/g after 5 minutes at 120° C.

13. A passive NO_x adsorbent according to claim 1 in which the mixed or composite oxide includes Mn as said at least one transition metal and optional Ce, with a minimum aged NO_x storage capacity of at least 19 μmol/g after 5 minutes at 120° C.

14. A passive NO_x adsorbent according to claim 1 in which the mixed or composite oxide includes Mn as said at least one transition metal, with a minimum fresh NO_x storage capacity of at least 50 μmol/g after 5 minutes at 120° C.

15. A passive NO_x adsorbent according to claim 1 in which the mixed or composite oxide includes Mn as said at least one transition metal, with a minimum aged NO_x storage capacity of at least 45 μmol/g after 5 minutes at 120° C.

16. A passive NO_x adsorbent according to claim 1 in combination with a Selective Catalytic Reduction catalyst.

17. A monolithic substrate supporting a washcoat, said washcoat comprising said passive NO_x adsorbent according to claim 1.

18. A method for reducing nitrogen oxides (NO_x) present in a lean gas stream comprising at least one of nitric oxide (NO) and nitrogen dioxide (NO₂), comprising the steps of:

- (i) providing the passive NO_x adsorbent according to claim 1 in the lean gas stream;
- (ii) adsorbing NO_x from the lean gas stream on or in the passive NO_x adsorbent at a temperature below 200° C.;
- (iii) thermally net desorbing NO_x from the passive NO_x adsorbent in the lean gas stream at 200° C. and above;
- (iv) catalytically reducing the NO_x on a downstream catalyst situated downstream of the passive NO_x adsorbent, with at least one of the following reductants: a nitrogenous reductant, a hydrocarbon reductant, hydrogen and a mixture thereof.

19. A method according to claim 18 wherein the lean gas stream emanates from a gasoline fueled or diesel fueled engine.

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